

46.41 A 7lb_m cast iron pan ($c_p = 0.1 \frac{\text{Btu}}{\text{lb}_m \text{ } ^\circ\text{F}}$) is heated uniformly to 500°F during cooking, then placed in a sink filled with 4 gallons of 60°F water. Neglecting losses, what is the final equilibrium temperature?

- A. 69°F
- B. 79°F
- C. 89°F
- D. 99°F

All of the heat released from the pan is added to the water. Express both quantities of heat as the product of mass, specific heat capacity, and ΔT . Set them equal.

$$(mc_p\Delta T)_{\text{iron}} = (mc_p\Delta T)_{\text{water}}$$

In the case of water, the volume was given instead of the mass. Use the density of water to calculate the mass.

$$m_{\text{water}} = \rho V = \left(62.4 \frac{\text{lb}_m}{\text{ft}^3}\right) \left(\frac{1\text{ft}^3}{7.48\text{gal}}\right) (4\text{gal}) = 33.4\text{lb}_m$$

Substitute into the first equation and solve for the final equilibrium temperature, T_f , which is the same for the pan and the water.

$$(7\text{lb}_m) \left(0.1 \frac{\text{Btu}}{\text{lb}_m \text{ } ^\circ\text{F}}\right) (500^\circ\text{F} - T_f) = (33.4\text{lb}_m) \left(1 \frac{\text{Btu}}{\text{lb}_m \text{ } ^\circ\text{F}}\right) (T_f - 60^\circ\text{F})$$

Since the units are all consistent, it is fine to ignore the units while solving for the unknown temperature.

$$(0.7) (500 - T_f) = (33.4) (T_f - 60)$$

$$350 - 0.7T_f = 33.4T_f - 2002$$

$$2352 = 34.1T_f$$

$$T_f = 69^\circ\text{F}$$

Answer A

46.42 A refrigeration system using R-22 operates between $80^\circ F$ condensing and $0^\circ F$ evaporation. The refrigerant exits the evaporator as a dry, saturated vapor. What is the specific work done by the compressor assuming isentropic compression?

- A. $9 \frac{Btu}{lb}$
- B. $11 \frac{Btu}{lb}$
- C. $15 \frac{Btu}{lb}$
- D. $18 \frac{Btu}{lb}$

Draw the refrigeration cycle on the Pressure-Enthalpy diagram for Refrigerant 22, labelling all 4 States. The compression process is from State 1 to State 2. The specific work done by the compressor is the difference between the enthalpy at State 2 and the enthalpy at State 1. Specific work is distinct from 'Work' in that its units are $\frac{Btu}{lb}$ (as opposed to $\frac{Btu}{hr}$) and it does not require the mass flow rate.

$$Work = \dot{W}_{comp} = \dot{m}\Delta h = \dot{m}(h_2 - h_1)$$

$$Specific\ Work = w = h_2 - h_1$$

Start by analyzing State 1 which is a dry, saturated vapor with a known Temperature. Use the [Refrigerant 22](#) table to obtain the enthalpy at State 1.

$$T_1 = 0^\circ F$$

$$h_1 = h_f = 104.6 \frac{Btu}{lb}$$

Use the [Pressure Versus Enthalpy Curves for Refrigerant 22](#) to locate State 1. Since the compression process is isentropic, draw a line of constant entropy up and to the right.

The condensing temperature is $80^\circ F$, which is implied to refer to the segment of the condensing process line which lies inside the vapor dome. The condensing process is constant *pressure* throughout the entire process, however it is only constant *temperature* inside the vapor dome. Extend a horizontal line to the right from the $80^\circ F$ line.

Graphically locate State 2 as the intersection of the extended $80^\circ F$ line and the constant entropy line previously drawn from State 1. Read the enthalpy at State 2 along the top horizontal axis. Some uncertainty and imprecision is to be expected due to graphical nature of this approach.

$$h_2 \approx 120 \frac{Btu}{lb}$$

Calculate the specific work.

$$w = 120 \frac{Btu}{lb} - 104.6 \frac{Btu}{lb} = 15.4$$

Answer C