

47.20 A refrigeration cycle using R-123 operates between 75psia and 220psia with no sub-cooling. During isenthalpic expansion, what is the change in entropy of the refrigerant?

- A. $0.001 \frac{\text{Btu}}{\text{lb}\cdot^\circ\text{F}}$
- B. $0.003 \frac{\text{Btu}}{\text{lb}\cdot^\circ\text{F}}$
- C. $0.01 \frac{\text{Btu}}{\text{lb}\cdot^\circ\text{F}}$
- D. $0.04 \frac{\text{Btu}}{\text{lb}\cdot^\circ\text{F}}$

Sketch the process line from State 3 to State 4 representing the expansion process within a typical refrigeration cycle. Use the table for **Refrigerant 123** to obtain the enthalpy and entropy at State 3. Since there is no sub-cooling, the refrigerant is a saturated liquid at State 3.

$$P_3 = 220\text{psia}$$

$$h_3 = h_f = 78.66 \frac{\text{Btu}}{\text{lb}}$$

$$s_3 = s_f = 0.138 \frac{\text{Btu}}{\text{lb}\cdot^\circ\text{R}}$$

The expansion from $3 \rightarrow 4$ is isenthalpic, therefore the enthalpy at State 4 is the same as the enthalpy at State 3.

$$h_4 = h_3 = 78.66 \frac{\text{Btu}}{\text{lb}}$$

Since the expansion process line from $3 \rightarrow 4$ is vertically down on the Pressure-Enthalpy diagram, State 4 is observed to be a saturated mixture, as it is within the vapor dome. Use the Refrigerant 123 table again to obtain the enthalpy values h_f and h_{fg} at the lower pressure of State 4. Calculate the quality at State 4. Refer to **Properties for Two-Phase (Vapor-Liquid) Systems** for a reminder of the formulas involving quality.

$$P_4 = 75\text{psia}$$

$$h_f = 53.58 \frac{\text{Btu}}{\text{lb}}$$

$$h_{fg} = 115.68 \frac{\text{Btu}}{\text{lb}}$$

$$h_4 = h_f + \chi_4 h_{fg}$$

$$\chi_4 = \frac{h_4 - h_f}{h_{fg}} = \frac{78.66 \frac{\text{Btu}}{\text{lb}} - 53.58 \frac{\text{Btu}}{\text{lb}}}{115.68 \frac{\text{Btu}}{\text{lb}}} = 0.404$$

Use the same line in the table to obtain the entropy values s_f and s_{fg} . Calculate the entropy at State 4 using the quality, χ_4 .

$$s_f = 0.102 \frac{\text{Btu}}{\text{lb}^\circ\text{R}}$$

$$s_{fg} = 0.199 \frac{\text{Btu}}{\text{lb}^\circ\text{R}}$$

$$s_4 = s_f + \chi_4 s_{fg} = \left(0.102 \frac{\text{Btu}}{\text{lb}^\circ\text{R}}\right) + (0.404) \left(0.199 \frac{\text{Btu}}{\text{lb}^\circ\text{R}}\right) = 0.182 \frac{\text{Btu}}{\text{lb}^\circ\text{R}}$$

Finally, calculate the change in entropy during the expansion process.

$$\Delta s = s_4 - s_3 = 0.182 \frac{\text{Btu}}{\text{lb}^\circ\text{R}} - 0.138 \frac{\text{Btu}}{\text{lb}^\circ\text{R}} = 0.044 \frac{\text{Btu}}{\text{lb}^\circ\text{R}}$$

Answer D

47.21 A flash distillation vessel boils seawater to make potable water. The pressure in the vessel is held at 10 in Hg vacuum. What temperature does the seawater boil at?

- A. 162°F
- B. 192°F
- C. 212°F
- D. 228°F

Convert the pressure in the vessel to absolute terms of *psia*, using conversions from the [Measurement Relationships](#) table as needed. Recall that vacuum pressure reads negative on a gauge, but pressure is always positive in absolute terms.

$$P_g = (-10 \text{ in Hg}) \left(\frac{1 \text{ psi}}{2.036 \text{ in Hg}} \right) = -4.91 \text{ psig}$$

$$P_a = P_g + 14.7 \text{ psi} = -4.91 \text{ psig} + 14.7 \text{ psi} = 9.8 \text{ psia}$$

Use the [Properties of Saturated Water and Steam](#) table to look up the saturation temperature at 9.8 *psia*. The saturation temperature is the boiling point of water at a given pressure. As a sense check, the boiling point should be *lower* than at standard conditions since there is less pressure holding the molecules from escaping.

$$T_{sat@9.8 \text{ psia}} \approx 192^\circ\text{F}$$

Ignore boiling point elevation; salinity accounts for only about +1°F and is outside the intended scope of the problem.

Answer B