



$$\frac{N_{air}}{N_{fuel}} = \frac{2 + 2(3.77)}{1} = 9.54 \frac{moles_{air}}{moles_{fuel}} = 9.54 \frac{ft^3_{air}}{ft^3_{fuel}}$$

$$\frac{m_{air}}{m_{fuel}} = \frac{9.54(29)}{1(16)} = 17.29 \frac{lb_{air}}{lb_{fuel}}$$

Calculate the mass of air based on the mass of fuel given, the air-to-fuel ratio, and the amount of excess air.

$$m_{air} = (25lb_{fuel}) \left( 17.29 \frac{lb_{air}}{lb_{fuel}} \right) (1.3) = 562lb_{air}$$

**Answer D**

**47.78** During the process of condensing in a counterflow heat exchanger, the enthalpy of R-410A is reduced from  $125 \frac{Btu}{lb}$  to  $42 \frac{Btu}{lb}$ . The cooling medium is water which enters at  $50^\circ F$  and exits at  $75^\circ F$ . The surface area of the heat exchanger is  $40ft^2$  and the overall coefficient of heat transfer is  $10 \frac{Btu}{hr \cdot ft^2 \cdot ^\circ F}$ . What is the mass flow rate of refrigerant being condensed?

- A.  $36 \frac{lb}{hr}$
- B.  $41 \frac{lb}{hr}$
- C.  $46 \frac{lb}{hr}$
- D.  $51 \frac{lb}{hr}$

Search for **Heat Exchangers** and use the formula for the rate of heat transfer in the condenser. Assume  $F = 1$ . The overall coefficient of heat transfer,  $U$ , is given. The area,  $A$ , is given.

$$\dot{Q} = UAF\Delta T_{lm}$$

To determine the **Log Mean Temperature Difference**,  $\Delta T_{lm}$ , sketch the water cooled condenser and label the entering and exiting refrigerant and water temperatures. Use the **Refrigerant 410A** table and observe that for the condenser exit condition corresponding to State 3 of the refrigeration cycle,  $h_3 = 42 \frac{Btu}{lb}$ , therefore  $P_3 \approx 240psia$  and  $T_3 \approx 77^\circ F$ . The temperature of the refrigerant throughout the condenser is approximately constant as it is undergoing a phase change at constant pressure.

$$77^\circ F \longleftarrow 77^\circ F$$

$$50^\circ F \longrightarrow 75^\circ F$$

Calculate the temperature differential on each physical side of the exchanger, arbitrarily labeling the sides A & B.

$$\Delta T_A = 77^\circ F - 50^\circ F = 27^\circ F$$

$$\Delta T_B = 77^\circ F - 75^\circ F = 2^\circ F$$

Calculate the **Log Mean Temperature Difference**,  $\Delta T_{lm}$ . The formula below is consistent with the formula shown in the reference handbook, but may be easier to correctly apply once the temperature differentials are properly defined. Note that interchanging  $\Delta T_A$  and  $\Delta T_B$  leads to the same correct result!

$$\Delta T_{lm} = \frac{\Delta T_A - \Delta T_B}{\ln\left(\frac{\Delta T_A}{\Delta T_B}\right)}$$

$$\Delta T_{lm} = \frac{27^\circ F - 2^\circ F}{\ln\left(\frac{27^\circ F}{2^\circ F}\right)} = 9.6^\circ F$$

Calculate the heat transfer through the heat exchanger.

$$\dot{Q} = UAF\Delta T_{lm} = \left(10 \frac{Btu}{hr \cdot ft^2 \cdot ^\circ F}\right) (40 ft^2) (1) (9.6^\circ F) = 3840 \frac{Btu}{hr}$$

Equate the heat transfer through the heat exchanger to the quantity of heat given up by the refrigerant, which is a function of the unknown mass flow rate,  $\dot{m}_r$ , and the change in enthalpy,  $\Delta h$ , of the refrigerant as it flows through the condenser.

$$\dot{Q} = \dot{m}_r (h_2 - h_3)$$

$$\dot{m}_r = \frac{\dot{Q}}{(h_2 - h_3)} = \frac{3840 \frac{Btu}{hr}}{\left(125 \frac{Btu}{lb} - 42 \frac{Btu}{lb}\right)} = 46.3 \frac{lb}{hr}$$

**Answer C**